

DOCTORAL THESIS

The catalytic performance and characterization of BaO- and BaX₂(X=F, Cl, Br)-promoted Ln₂O₃(Ln=Y, Er, Nd) catalysts for the oxidative coupling of methane

Liu, Yiwei

Date of Award:
1998

[Link to publication](#)

General rights

Copyright and intellectual property rights for the publications made accessible in HKBU Scholars are retained by the authors and/or other copyright owners. In addition to the restrictions prescribed by the Copyright Ordinance of Hong Kong, all users and readers must also observe the following terms of use:

- Users may download and print one copy of any publication from HKBU Scholars for the purpose of private study or research
- Users cannot further distribute the material or use it for any profit-making activity or commercial gain
- To share publications in HKBU Scholars with others, users are welcome to freely distribute the permanent URL assigned to the publication

(5634176

TH
PH.D.
1998 LC

**The Catalytic Performance and
Characterization of BaO- and BaX₂(X = F, Cl,
Br)-Promoted Ln₂O₃ (Ln = Y, Er, Nd) Catalysts
for the Oxidative Coupling of Methane**

LIU Yiwei

A thesis submitted in partial fulfilment of the requirements

for the degree of

Doctor of Philosophy

July 1998

Hong Kong Baptist University

ABSTRACT

In this work, the catalytic performances of BaO- and BaX₂(X=F, Cl, Br)-promoted Ln₂O₃ (Ln=Y, Er, Nd) catalysts have been investigated systematically for the oxidative coupling of methane (OCM). The bulk composition, crystal structure, surface composition, surface area, surface active oxygen species of the catalysts, and the activity of various oxygen species were examined by techniques such as X-ray diffraction (XRD), X-ray photoelectron spectroscopy (XPS), temperature programmed desorption (TPD), temperature programmed reduction (TPR), CH₄- and O₂-pulsing experiments, Raman spectrometry, and electron paramagnetic resonance (EPR).

The performances of the 30 mol% MO/Y₂O₃ (M = Mg, Ca, Sr, Ba) catalysts for the OCM reaction have been explored. The BaO-promoted catalysts showed the best activity. When BaX₂ (X= F, Cl, Br) was used instead of BaO for the modification of Y₂O₃, the reactivities could be improved significantly, especially in C₂ selectivity and C₂H₄/C₂H₆ ratio. The 30 mol% BaCl₂/Y₂O₃ catalysts showed a C₂ yield of 22.3% at 800°C with CH₄ : O₂ : N₂ = 2.47 : 1 : 11.4, total flow rate = 50 mL min⁻¹, contact time = 0.6 g s mL⁻¹, and catalyst weight = 0.5 g. The XRD results revealed that the addition of 10-50 mol% of BaO or BaCl₂ could greatly alter the surface and bulk natures of Y₂O₃. The cubic Y₂O₃ lattices in BaO- and BaCl₂-promoted Y₂O₃ catalysts were found to have undergone

expansion which resulted from ionic substitution between Ba^{2+} and Y^{3+} ions. The reactivity of the 30 mol% $\text{BaCl}_2/\text{Y}_2\text{O}_3$ catalyst was stable within 40 h of reaction at 750°C . Although the analysis of chlorine content indicated that there was leaching of Cl^- ions, XPS results revealed no change in surface chlorine concentration. O_2 -TPD and reduction studies of the fresh 30 mol% BaO - and BaCl_2 -promoted catalysts showed that the amount of active oxygen in the former was at least 4 times that in the latter. It was apparent that the presence of Ba^{2+} ions could enhance the amount of surface oxygen species, while the presence of Cl^- could inhibit the deep oxidation reactions.

The BaF_2 -promoted Y_2O_3 catalysts also exhibited good performance. A conversion of 36.1% and a selectivity of 62.1% were achieved at 750°C over the 95 mol% $\text{BaF}_2/\text{Y}_2\text{O}_3$ catalyst, the corresponding yield was 22.4%. The XRD results showed that the cubic Y_2O_3 lattice expanded slightly while the cubic BaF_2 lattice contracted. It is suggested that there were substitutions between the Ba^{2+} and Y^{3+} ions as well as the F^- and O^{2-} ions. Such ionic substitutions could result in the generation of active lattice defects such as anion vacancies, trapped electrons, and charge-deficient oxygen species. The EPR experiments confirmed the generation of trapped electrons in the 95 mol% $\text{BaF}_2/\text{Y}_2\text{O}_3$ catalyst. After H_2 reduction between 500 and 700°C , a kind of trapped electrons with EPR signal centered at 2.0871 was detected. H_2 reduction above 700°C could result in the generation of another type of trapped electrons with EPR signal centered at

2.0087. The 2.0871 signal showed doublet superhyperfine structure while the 2.0087 one was symmetrical. The former was interpreted as being due to trapped electrons interacting with the Y^{3+} ions, whereas the latter was due to trapped electrons shared among the orbitals of the surrounding cations. The 2.0871 trapped electrons spread throughout the sample, while the 2.0087 ones existed only on the surface. The involvement of surface-trapped electrons in activating O_2 was observed at $25^\circ C$, while above $500^\circ C$, trapped electrons in the bulk were also involved. According to the results, we concluded that in the OCM reaction, the BaF_2/Y_2O_3 catalysts were reduced by hydrogen dissociated from methane and trapped electrons were generated. These trapped electrons could serve as active sites for O_2 activation.

The BaO - and BaX_2 -promoted Er_2O_3 catalysts have also been investigated for the OCM reaction. The $BaCl_2$ -promoted Er_2O_3 catalysts showed very good performance. At $750^\circ C$ with $CH_4/O_2 = 2.2$, the 30 mol% $BaCl_2/Er_2O_3$ catalyst showed the highest yield of 26.2%. The highest C_2H_4/C_2H_6 ratio was 20.6 at $800^\circ C$ with $CH_4/O_2 = 2.47$. On the basis of XRD, XPS, Raman, and TPR results, one can conclude that the Ba^{2+} and X^- ions were involved in promoting Er_2O_3 . According to the chemical analysis results, the stability of halide ions in the catalysts followed the sequence of $F^- > Cl^- > Br^-$. The F^- ions tend to diffuse into the bulk whereas the Cl^- and Br^- ions migrate to the surface of the catalyst. Although losses of Cl^- and Br^- ions occurred during the reaction, XPS studies indicated no changes in the surface concentrations of Cl^- and Br^- ions. The Raman results

showed that no dioxygen species existed on the surface of undoped Er_2O_3 , while there were dioxygen species such as O_2^{2-} , O_2^{n-} , O_2^- , and $\text{O}_2^{\delta-}$ on the BaO- and BaX_2 -promoted catalysts. The formation of dioxygen species on the surfaces was due to the interaction of lattice defects with gaseous O_2 . Based on the Raman and TPR results, we conclude that the reducible oxygen species in these catalysts were composed of both dioxygen and mono-oxygen species. The presence of dioxygen inhibits the deep oxidation of hydrocarbons, causing the C_2 selectivity and $\text{C}_2\text{H}_4/\text{C}_2\text{H}_6$ ratio to increase.

The 30 mol% BaO- and 30 mol% BaX_2 -promoted Nd_2O_3 catalysts performed better than the undoped Nd_2O_3 catalyst. This is due to the fact that the addition of BaO and BaX_2 to Nd_2O_3 caused the formation of lattice defects which facilitates the production of active oxygen adspecies such as O_2^{2-} , O_2^{n-} , O_2^- , and $\text{O}_2^{\delta-}$ on the surfaces. The TPR results suggested that besides the dioxygen adspecies, there was mono-oxygen on the surfaces. The CH_4 -pulsing and Raman experiments demonstrated that both the mono-oxygen and dioxygen adspecies could activate CH_4 at higher temperatures but the former was more active than the latter in the deep oxidation of hydrocarbons.

CONTENTS

DECLARATION	i
ABSTRACT	ii
ACKNOWLEDGMENTS	vi
CONTENTS	vii
LIST OF TABLES	xii
LIST OF FIGURES	xv
CHAPTER 1 INTRODUCTION	1
1.1 Methane Utilization	1
1.2 Catalysts	3
1.2.1 Alkaline Earth Oxide	5
1.2.2 Rare earth Oxide	6
1.2.3 Modification of Rare Earth Oxide Catalysts by Cations	7
1.2.4 Modification of Catalysts by Anions	9
1.3 Mechanism for Methane Activation	12
1.3.1 C-H Cleavage	12
1.3.2 Oxygen Species or Active Centers for Methane Activation	15
1.4 Reaction Mechanism	21
1.5 Background of Studies	24
References	26
CHAPTER 2 EXPERIMENTAL	34
2.1 Preparation of Catalysts	34
2.2 Testing System	34
2.3 Catalyst Characterization	37

2.3.1 Surface Area Measurement	37
2.3.2 Structure Measurement	38
2.3.3 X-Ray Photoelectron Spectroscopic (XPS) Studies	40
2.3.4 Temperature Programmed Desorption (TPD)	41
2.3.5 Halide Analysis	41
2.3.6 $^{18}\text{O}/^{16}\text{O}$ Isotope Exchange	42
2.3.7 Temperature Programmed Reduction (TPR)	43
2.3.8 O_2 Pulse Experiment	43
2.3.9 CH_4 Pulse Experiment	44
2.3.10 Laser Raman Spectrometry	44
2.3.11 Electron Paramagnetic Resonance (EPR)	45
References	45
CHAPTER 3 THE MAKING AND CHARACTERIZATION OF BaO- AND BaCl_2 -PROMOTED Y_2O_3 CATALYSTS FOR THE OCM REACTION	46
3.1 Introduction	46
3.2 Results	49
3.2.1 Catalytic Performance of Y_2O_3 and MO ($M=\text{Mg}, \text{Ca}, \text{Sr}, \text{Ba}$)- Promoted Y_2O_3 Catalysts	49
3.2.2 Catalytic Performance of BaX_2 ($X=\text{F}, \text{Cl}, \text{Br}$)-Promoted Y_2O_3 Catalysts	51
3.2.3 Effects of BaCl_2 and BaO Loadings on the $\text{BaO}/\text{Y}_2\text{O}_3$ and $\text{BaCl}_2/\text{Y}_2\text{O}_3$ Catalysts	53
3.2.4 BET, XRD, and XPS Studies	56
3.2.5 Performance of 30 mol% $\text{BaCl}_2/\text{Y}_2\text{O}_3$ as Related to Reaction Time, Contact Time, and CH_4/O_2 Ratio	60

3.2.6	O ₂ and CO ₂ TPD Studies of BaO/Y ₂ O ₃ and BaCl ₂ /Y ₂ O ₃	63
3.2.7	¹⁸ O/ ¹⁶ O Isotope Exchange over Y ₂ O ₃ , 30 mol% BaO/Y ₂ O ₃ , and 30 mol% BaCl ₂ /Y ₂ O ₃	70
3.2.8	Reduction Studies of Y ₂ O ₃ , 30 mol% BaO/Y ₂ O ₃ , and 30 mol% BaCl ₂ /Y ₂ O ₃	70
3.3	Discussion	73
3.4	Conclusions	79
	References	80
CHAPTER 4 THE CHARACTERIZATION OF BaF ₂ /Y ₂ O ₃ CATALYSTS FOR THE OCM REACTION		84
4.1	Introduction	84
4.2	Results	87
4.2.1	Catalytic Activities and BET Measurements	87
4.2.2	XRD and XPS Studies	91
4.2.3	TPR and Raman Studies	96
4.2.4	EPR Studies	99
4.2.5	O ₂ -Pulsing Studies	103
4.3	Discussion	105
4.4	Conclusions	112
	References	113
CHAPTER 5 THE MODIFICATION OF Er ₂ O ₃ WITH MO (M = Mg, Ca, Sr, Ba) AND BaX ₂ (X = F, Cl, Br), RESPECTIVELY, FOR THE OCM REACTION		116
5.1	Introduction	116

5.2 Results	117
5.2.1 Catalytic Performance of Er_2O_3 and MO ($M = \text{Mg, Ca, Sr, Ba}$)-Promoted Er_2O_3 Catalysts	117
5.2.2 Catalytic Performance of BaX_2 ($X = \text{F, Cl, Br}$)-Promoted Er_2O_3 Catalysts	120
5.2.3 Effects of BaO , BaF_2 , and BaCl_2 Loading on the $\text{BaO}/\text{Er}_2\text{O}_3$, $\text{BaF}_2/\text{Er}_2\text{O}_3$, and $\text{BaCl}_2/\text{Er}_2\text{O}_3$ Catalysts	121
5.2.4 XRD and XPS, and Halogen Analyses	125
5.2.5 The Effects of Reaction Time, Contact Time and CH_4/O_2 Ratio	129
5.2.6 O_2 TPD and Raman Studies of Er_2O_3 , 30 mol% $\text{BaO}/\text{Er}_2\text{O}_3$, and 30 mol% $\text{BaX}_2/\text{Er}_2\text{O}_3$	135
5.2.7 TPR Studies	143
5.2.8 Interaction of CH_4 with Oxygen Species	146
5.2.9 O_2 -Pulsing Studies	147
5.3 Discussion	149
5.4 Conclusions	156
References	157

CHAPTER 6 RAMAN SPECTROSCOPIC AND TPR STUDIES OF OXYGEN SPECIES OVER BaO - AND BaX_2 ($X = \text{F, Cl, Br}$)-PROMOTED Nd_2O_3 CATALYSTS FOR THE OXIDATIVE COUPLING OF METHANE 159

6.1 Introduction	159
6.2 Results	160
6.2.1 Catalytic Performances of BaO - and BaX_2 -Promoted Nd_2O_3 Catalysts	160
6.2.2 BET, XRD, and XPS Studies	162

6.2.3 Effects of BaCl ₂ Loading and Reaction Time on Catalytic Performance of BaCl ₂ -Promoted Nd ₂ O ₃ Catalysts	166
6.2.4 Raman Studies	168
6.2.5 TPR Studies	173
6.2.6 Interaction of CH ₄ with oxygen Species	175
6.2.7 O ₂ -Pulsing Studies	178
6.3 Discussion	180
6.4 Conclusions	186
References	187
CHAPTER 7 GENERAL CONCLUSIONS AND FUTURE WORK	188
7.1 General Conclusions	188
7.2 Future Work	191
CURRICULUM VITAE	193